

manufactured and sold by Showa Denko K.K.,
Japan) :--

Please replace the paragraph beginning on page 33, line 18 to
page 35, line 2 with the following rewritten paragraph:

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A --A preferred PTMG used in the present invention as the
component (B) has a number average molecular weight of from 500 to
3,000, a molecular weight distribution (M_w/M_n) of 1.75 or less, a
content of high molecule weight PTMG molecules of from 2 to 5% by
weight, and a heteropolyacid content of from 10 to 900 ppb by
weight. Following is a method for producing such a preferred PTMG
from THF using a heteropolyacid catalyst. In a reaction system
where water is present in an amount sufficient to form a THF
organic phase and an aqueous THF/catalyst phase having a specific
gravity of from 1.8 to 2.3, the retention time (V/F) of THF is
maintained within the range of from 0.5 to 20 hours, preferably
from 0.7 to 15 hours. When the V/F value is smaller than the
above-mentioned range, the conversion of THF is likely to become
low. On the other hand, when the V/F value is larger than the
above-mentioned range, the reaction time is likely to become long.
With respect to the motive power (P/V) applied to the liquid in
the reactor, the P/V value is maintained at 1.3 kW/m^3 or more,
preferably 1.6 kW/m^3 or more. When the P/V is smaller than 1.3
 kW/m^3 , the agitation of the reaction system becomes unsatisfactory
and the distribution of the diameters of the globules in the
reaction system become broad. As a result, the molecular weight

distribution of the produced PTMG becomes broad and the control of the molecule weight distribution of the PTMG becomes difficult. By appropriately controlling the V/F and P/V values in the above-mentioned method, it is also possible to obtain a PTMG having a number average molecular weight of more than 3,000 and less than or equal to 4,000, and a content of high molecular weight PTMG molecules of more than 5 % by weight and less than or equal to 10 % by weight.--

Please replace the paragraph beginning on page 65 line 17 to page 66, line 15 with the following rewritten paragraph:

--First, a heteropolyacid catalyst solution for use as a polymerization catalyst was produced as follows. A 2-liter reaction vessel was prepared, which is provided with a 3-way cock having three respective ends, wherein each end has attached thereto a condenser and an eggplant type flask for collecting and storing a distillate produced by the condenser, so that the contents of the reaction vessel can be distilled. The thus prepared reaction vessel was used for producing a heteropolyacid catalyst solution. 1 liter of tetrahydrofuran (THF) and 600 g of silicotungstic acid dodecahydrate were introduced into the reaction vessel in this order, and stirred at 60°C, while continuously removing an azeotropic vapor of water and THF from the reaction vessel. The specific gravity of a solution being formed in the reaction vessel was periodically measured while feeding THF to the reaction vessel every 10 minutes so as to

compensate for the total amount of water and THF removed from the reaction vessel. When the specific gravity of the solution became 2.07, the reaction was terminated to thereby obtain a catalyst solution having a specific gravity of 2.07, namely a solution of heteropolyacid catalyst in a THF/water mixture.--

Please replace the paragraph being on page 70, line 2 with the following rewritten paragraph:

--The obtained PTMG (A) had a number average molecular weight (Mn) of 1840, a molecular weight distribution (Mw/Mn) of 1.60, and a content of high molecular weight PTMG molecules which are at least six times as large as the number average molecular weight of all PTMG molecules (hereinafter, simply referred to as "content of high molecular weight PTMG molecules") of 2.29 % by weight. The number average molecular weight was determined by the terminal titration method, and the molecular weight distribution and the content of high molecular weight PTMG molecules were determined by gel permeation chromatography (GPC) under the conditions mentioned below.--

Please replace the paragraph beginning at page 71, line 21 as with the following rewritten paragraph:

AG
--Columns: Shodex OH pak (manufactured and sold by Showa
Denko K.K., Japan):
SB 806 M (2 columns)
SB 802.5 (1 column) --